APS Educational Trust®

A P S College of Engineering

(Approved by AICTE & Affiliated to VTU) 26th km,
NH-209, Kanakapura road, Bengaluru-82

Department of Mechanical Engineering

Laboratory Manual

HEAT TRANSFER LABORATORY

HEAT TRANSFER LABORATORY

IA Marks : 40
Hours/Week : 03 **Exam Hours : 03**

PART – A

1. Determination of Thermal Conductivity of a Metal Rod.
2. Determination of Overall Heat Transfer Coefficient of a Composite wall.
3. Determination of Effectiveness on a Metallic fin.
4. Determination of Heat Transfer Coefficient in a free Convection on a vertical tube.
5. Determination of Heat Transfer Coefficient in a Forced Convention Flow through a Pipe.
6. Determination of Emissivity of a Surface.

PART – B

1. Determination of Steffan Boltzman Constant.
2. Determination of LMDT and Effectiveness in a Parallel Flow and Counter Flow Heat Exchangers
3. Experiments on Boiling of Liquid and Condensation of Vapour
4. Performance Test on a Vapour Compression Refrigeration.
5. Performance Test on a Vapour Compression Air - Conditioner
6. Experiment on Transient Conduction Heat Transfer

Scheme for Examination:

One Question from Part A - 40 Marks

One Question from Part B - 40 Marks

Viva-Voce - 20 Marks

Total: 100 Marks

Date:
Exp No:

COMPOSITE WALL APPARATUS

AIM:

To find out total thermal resistance and total thermal conductivity of Composite wall.

DESCRIPTION:

The apparatus consists of central heater sandwiched between the slabs of MS, Asbestos and Wood, which forms composite structure. The whole structure is well tightened make perfect contact between the slabs. A dimmer stat is provided to vary heat input of heaters and it is measured by a digital volt meter and ammeter. Thermocouples are embedded between interfaces of slabs. A digital temperature indicator is provided to measure temperature at various points.

SPECIFICATION:

1. Slab assembly arranged symmetrically on both sides of the Heater.
2. Heater coil type of 250-Watt capacity.
3. Dimmer stat open type, 230V, 0-5 amp, single phase.
4. Volt meter range 0-270V
5. Ammeter range 0-20A
6. Digital temperature indicator range 0-800^0 c
7. Thermocouple used: Teflon coated, Chromal - Alumal
8. Slab diameter of each =150 mm.
9. Thickness of mild steel = 10 mm.
10. Thickness of Asbestos = 6 mm.
11. Thickness of wood= 10 mm.

PROCEDURE:

1. Start the main switch.

2. By adjusting the dimmer knob give heat input to heater. (Say 60V).
3. Wait for about 20 -30 min. approximately to reach steady state.
4. Take the readings of all (8) thermocouples.
5. Tabulate the readings in observation table.
6. Make dimmer knob to “zero” position and then put main switch off.
7. Repeat the procedure for different heat input.

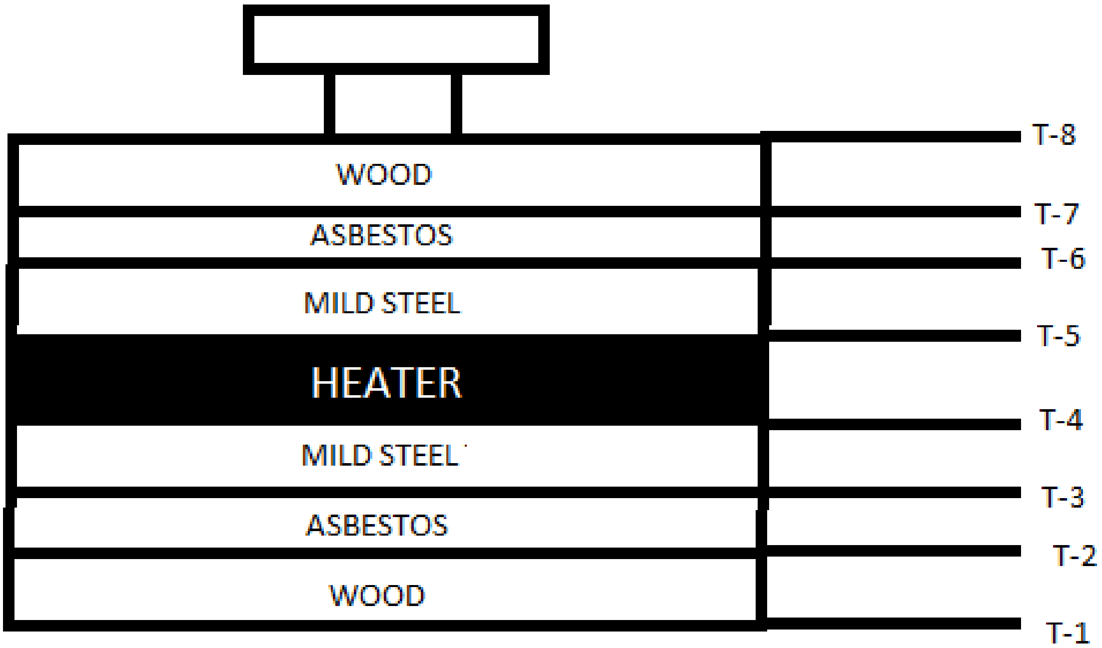


Fig :- COMPOSITE WALL

OBSERVATION TABLE:

Sl. No	V Volts	I amps	T_1 °C	T_2 °C	T_3 °C	T_4 °C	T_5 °C	T_6 °C	T_7 °C	T_8 °C
1.										
2.										
3.										

FORMULAE:

1. Heat input Q $= \dfrac{V \text{ X } I}{2}$ *Watts* ....

$$T_{Wood} = \frac{T_1 + T_8}{2} \quad °C \ldots\ldots\ldots\ldots\ldots\ldots$$

$$T_{Asbestos} = \frac{T_2 + T_7}{2} \quad °C \ldots\ldots\ldots\ldots\ldots..$$

$$T_{Mildsteel} = \frac{T_3 + T_6}{2} \quad °C \ldots\ldots\ldots\ldots\ldots\ldots$$

$$T_{Heater} = \frac{T_4 + T_5}{2} \quad °C \ldots\ldots\ldots\ldots\ldots\ldots..$$

2. Area of Slab

$$A = \frac{\prod d^2}{4} m^2$$ (Where "d" is diameter of slab= 300 mm)

3. Thermal Resistance of Slab (R)

$$R = \frac{T_{heater} - T_{wood}}{Q} \quad °C/W$$

4. Thermal Conductivity (K)

$$K = \frac{Q \times t}{A(T_{heater} - T_{wood})} \frac{W}{m-k}$$ (Where "t" is total thickness of slab=26mm)

<u>PRECAUTIONS</u>:

1. Keep the dimmer stat to zero before starting the experiment.
2. While removing plates do not disturb thermocouples.
3. Use the selector switch knob and dimmer knob gently.

<u>RESULT</u>:

1. Total thermal resistance of composite wall =……………………..

2. Total thermal conductivity of composite wall=…………

Date:

Exp No:

HEAT TRANSFER IN DROP AND FILM WISE CONDENSATION

AIM:

To determine the experimental and theoretical heat transfer coefficient for drop wise and film wise condensation.

INTRODUCTION:

Condensation of vapor is needed in many of the processes, like steam condensers, refrigeration etc. When vapor comes in contact with surface having temperature lower than saturation temperature, condensation occurs. When the condensate formed wets the surface, a film is formed over surface and the condensation is film wise condensation. When condensate does not wet the surface, drops are formed over the surface and condensation is drop wise condensation

APPARATUS:

The apparatus consists of two condensers, which are fitted inside a glass cylinder, which is clamped between two flanges. Steam from steam generator enters the cylinder through a separator. Water is circulated through the condensers. One of the condensers is with natural surface finish to promote film wise condensation and the other is chrome plated to create drop wise condensation. Water flow is measured by a Rota meter. A digital temperature indicator measures various temperatures. Steam pressure is measured by a pressure gauge. Thus heat transfer coefficients in drop wise and film wise condensation cab be calculated.

SPECIFICATIONS:

Heater	: Immersion type, capacity 2kW
Voltmeter	: Digital type, Range 0-300v
Ammeter	: Digital type, Range 0-20 amps
Dimmer stat	: 0-240 V, 2 amps
Temperature Indicator	: Digital type, 0-800°C

Thermocouple Used : Teflon coated, Chromal - Alumal (Ch-Al)

Diameter of copper tube d=16 mm

Length of copper tube L= 300 mm

Maximum Capacity of boiler : 2kg/cm^2

EXPERIMENTAL PROCEDURE:

1. Fill up the water in the steam generator and close the water-filling valve.
2. Start water supply through the condensers.
3. Close the steam control valve, switch on the supply and start the heater.
4. After some time, steam will be generated. Close water flow through one of the condensers.
5. Open steam control valve and allow steam to enter the cylinder and pressure gauge will show some reading.
6. Open drain valve and ensure that air in the cylinder is expelled out.
7. Close the drain valve and observe the condensers.
8. Depending upon the condenser in operation, drop wise or film wise condensation will be observed.
9. Wait for some time for steady state, and note down all the readings.
10. Repeat the procedure for the other condenser.

OBSERVATIONS:

'V' Volt	'I' Amp	Thermocouple readings (0C)								Volume flow rate of water, V cc/min
		T_1	T_2	T_3	T_4	T_5	T_6	T_7	T_8	

Water inlet temperature -T_1
Copper tube surface temperature (Film wise condensation) -T_2
Copper specimen chamber steam temperature - T_3
Gold tube surface temperature (Drop wise condensation) -T_4
Gold specimen chamber steam temperature - T_5
Steam Inlet temperature - T_6
Copper tube Water outlet temperature - T_7
Gold tube Water outlet temperature - T_8

CALCULATIONS:

(FILM WISE & DROP WISE CONDENSATION)

Water flow $m_w =$ kg/sec

Water inlet temperature = ^oC

Water outlet temperature = ^oC

(T_8 for drop-wise condensation and T_7 for film-wise condensation)

Heat carried away by the water,

$Q = m_w . c_P . (T_{7 \text{ or } 8} - T_1)$ Watts

Q=………… Watts

Where c_p = Specific heat of water = 4.2×10^3 J / Kg-K

Surface area of the condenser, $A = \pi dL$ m^2

Experimental heat transfer coefficient, $h = \dfrac{Q}{A(T_s - T_w)}$ $W / m^2 \, {}^oC$

(for both film wise and drop wise condensation)

Where T_s = Temperature of steam (T_3 or T_5)

T_W = Condenser wall temperature (T_2 or T_4)

Theoretically, for film wise condensation

$$h = 0.943 \left[\frac{h_{fg} . \rho^2 . g . k^3}{(T_s - T_w) . \mu . L} \right]^{0.25}$$

Where

h_{fg} = Latent heat of steam at T_S J/kg

(Take from temperature tables in steam tables)

ρ = Density of water, Kg / m^3

g = Gravitational acceleration, m / sec^2

k = Thermal conductivity of water W / m^o C

μ = Viscosity of water, N.s/m^2

L = Length of condenser = 0.15 m

Above values at mean temperature, $T_m = \dfrac{(T_s + T_W)}{2}$ ^oC (from data book)

(For drop wise condensation, determine experimental heat transfer coefficient only) In film wise condensation, film of water acts as barrier to heat transfer whereas, in case of drop formation, there is no barrier to heat transfer, Hence heat transfer coefficient in drop wise condensation is much greater than film wise condensation, and is preferred for condensation. But practically, it is difficult to prolong the drop wise condensation and after a period of condensation the surface becomes wetted by the liquid. Hence slowly film wise condensation starts.

PRECAUTIONS:

1. Operate all the switches and controls gently
2. Never allow steam to enter the cylinder unless the water is flowing through condenser.
3. Always ensure that the equipment is earthed properly before switching on the supply.

RESULTS:

Thus we studied and compared the drop wise and film wise condensation.

1. **Film wise condensation:**

   Experimental average heat transfer coefficient =

   Theoretical average heat transfer coefficient =

2. **Drop wise condensation:**

   Experimental average heat transfer coefficient =

   Theoretical average heat transfer coefficient =

Date:
Exp No:

EMISSIVITY MEASUREMENT OF RADIATING SURFACES

AIM:

To determine the emissivity of given test plate surface.

THEORY:

Any hot body maintained by a constant heat source, loses heat to surroundings by conduction, convection and radiation. If two bodies made of same geometry are heated under identical conditions, the heat loss by conduction and convection can be assumed same for both the bodies, when the difference in temperatures between these two bodies is not high. In such a case, when one body is black & the other body is gray from the values of different surface temperatures of the two bodies maintained by a constant power source emissivity can be calculated. The heat loss by radiation depends on

a) Characteristic of the material
b) Geometry of the surface and
c) Temperature of the surface

The heat loss by radiation when one body is completely enclosed by the other body is given by

$$Q = \frac{\sigma A_1 (T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{A_1}{A_2}\left[\frac{1}{\varepsilon_2} - 1\right]}$$

If a body is losing heat to the surrounding atmosphere, then the area of atmosphere A_2 >> area of body A_1. Thus if anybody is losing heat by radiation to the surrounding atmosphere equation (1) takes the form.

$$Q = \sigma A_1 (T_1^4 - T_2^4)$$

Where

σ = Stefan Boltzmannn constant = 5.6697×10^{-8} W/m² K⁴

A_1 = Surface area in m²

ε = Emissivity

T_1 = surface temperature of the body in K and

T_2 = surrounding atmospheric temperature in K

Let us consider a black body & a gray body with identical geometry being heated under identical conditions, assuming conduction & convection heat loss to remain the same.

Let Q_b and Q_g be the heat supplied to black & gray bodies respectively. If heat input to both the bodies are same,

$$Q_b = Q_g$$

Assuming, heat loss by conduction and convection from both bodies to remain same.

$$\boxed{\text{Heat loss by radiation by the black body = Heat loss by radiation by the gray body}}$$

$$\sigma A_b \varepsilon_b (T_b^4 - T_a^4) = \sigma A_g \varepsilon_g (T_g^4 - T_a^4)$$

As geometry of two bodies are identical A = A_g = A_b and ε_b = 1 for black body.

Therefore, $$\varepsilon_g = \frac{(T_b^4 - T_a^4)}{(T_g^4 - T_a^4)}$$

Where

Suffix 'b' stands for black body,

Suffix 'g' stands for gray body,

Suffix 'c' stands for chamber.

DESCRIPTION:

The experimental set up consists of two circular aluminium plates of identical dimensions. One of the plates is made black by applying a thick layer of lamp black while the other plate whose emissivity is to be measured is a gray body. Heating coils are provided at the bottom of the plates. The plates are mounted on asbestos cement sheet and kept in an enclosure to provide undisturbed natural convection condition. Three thermocouples are mounted on each plate to measure the average temperature. One thermocouple is in the chamber to measure the ambient temperature or chamber air temperature. The heat input can be varied with the help of variac for both the plates , that can be measured using digital volt and ammeter.

SPECIFICATIONS:

Specimen material : Aluminum

Specimen Size : ϕ 150 mm, 10 mm thickness (gray & black body)

Voltmeter : Digital type, 0-300v

Ammeter : Digital type, 0-3 amps

Dimmer stat : 0-240 V, 2 amps

Temperature Indicator : Digital type, 0-300°C, K type

Thermocouple Used : 7 nos.

Heater : Sand witched type Nichrome heater, 400 W

PROCEDURE:

1. Switch on the electric mains.
2. Operate the dimmer stat very slowly and give same power input to both the heater Say 60 V by using (or) operating cam switches provided panel.
3. When steady state is reached note down the temperatures T_1 to T_7 by rotating the temperature selection switch gently.
4. Also note down the volt & ammeter reading
5. Repeat the experiment for different heat inputs.

OBSERVATION TABLE:

Sl. No.	Heater input		Temperature of black surface °C			Temperature of gray surface °C			Chamber Temp °C
	V	I	T_1	T_2	T_3	T_5	T_6	T_7	T_4
1.									
2.									
3.									

SPECIMEN CALCULATIONS:

1. Temperature of the black body $T_b = \frac{(T_1 + T_2 + T_3)}{3} + 273.15$ K
2. Temperature of the gray body $T_g = \frac{(T_5 + T_6 + T_7)}{3} + 273.15$ K
3. Temperature of the Chamber $T_c = (T_7 + 273.15)$ K
4. Heat input to the coils Q = V x I watt
5. Emissivity of gray body $\varepsilon_g = \varepsilon_b \left[\frac{(T_b^4 - T_C^4)}{(T_g^4 - T_C^4)} \right]$

Result:

Emissivity of the black body is greater than gray body.

The emissivity of the test plate (gray body) surface is determined =………………..

Date:
Exp No:

HEAT TRANSFER BY FORCED CONVECTION

AIM:

To determine the convective heat transfer coefficient and the rate of heat transfer by forced convection for flow of air inside a horizontal pipe.

THEORY:

Convective heat transfer between a fluid and a solid surface takes place by the movement of fluid particles relative to the surface. If the movement of fluid particles is caused by means of external agency such as pump or blower that forces fluid over the surface, then the process of heat transfer is called forced convection.

In convectional heat transfer, there are two flow regions namely laminar & turbulent. The non-dimensional number called Reynolds number is used as the criterion to determine change from laminar to turbulent flow. For smaller value of Reynolds number viscous forces are dominant and the flow is laminar and for larger value of Reynolds numbers the inertia forces become dominant and the flow is turbulent. Dittus –Boelter correlation for fully developed turbulent flow in circular pipes is,

$$N_u = 0.023\,(Re)^{0.8}\,(Pr)^{n} \qquad \text{(from data book)}$$

Where

n = 0.4 for heating of fluid
n = 0.3 for cooling of fluid

Nusselt number= $N_u = \frac{hd}{k}$

R_e = Reynolds Number = $\frac{Vd}{\vartheta}$

P_r = Prandtl Number = $\frac{\mu C_P}{k}$

DESCRIPTION OF THE APPARATUS:

The apparatus consists of a blower to supply air. The air from the blower passes through a flow passage, heater and then to the test section. Air flow is measured by an orifice meter placed near the test section. A heater placed around the tube heats the air, heat input is controlled by a dimmer stat. Temperature of the air at inlet and at outlet are measured using thermocouples. The surface temperature of the tube wall is measured at different sections using thermocouples embedded in the walls. Test section is enclosed in a asbestos rope where the circulation of rope is avoid the heat loss to outside.

PROCEDURE:

1. Start the blower after keeping the valve open, at desired rate.
2. Put on the heater and adjust the voltage to a desired value and maintain it as constant
3. Allow the system to stabilize and reach a steady state.
4. Note down all the temperatures T_1 to T_7, voltmeter and ammeter readings, and manometer readings.
5. Repeat the experiment for different heat input and flow rates.

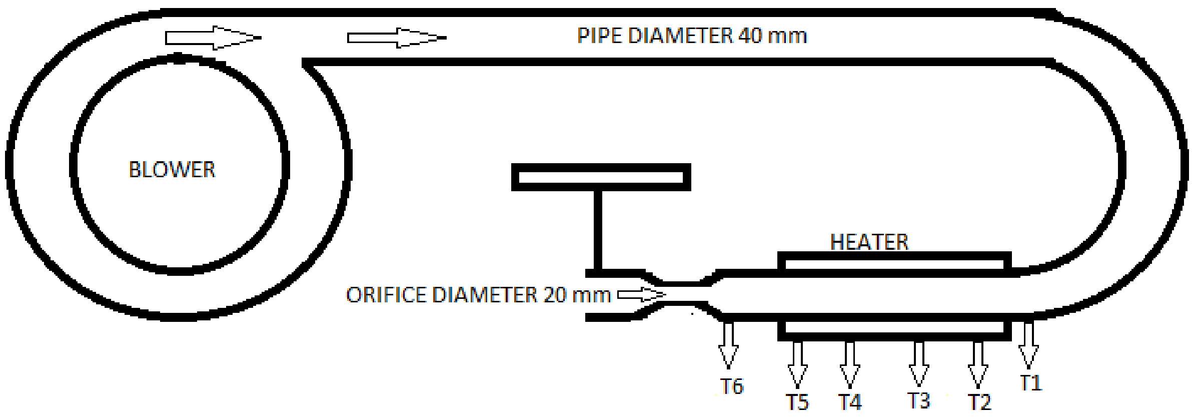


Fig:- FORCED CONVECTION APPARATUS

SPECIFICATIONS:

Specimen	: Copper Tube
Size of the Specimen	: I.D. 25mm x 300mm long
Heater	: Externally heated, Nichrome wire Band Heater
Ammeter	: Digital type, 0-20amps, AC
Voltmeter	: Digital type, 0-300volts, AC

Dimmer stat for heating Coil : 0-230v, 2amps

Thermocouple Used : 7 nos.

Centrifugal Blower : Single Phase 230v, 50 hz, 3000rpm

Manometer : U-tube with water as working fluid

Orifice diameter, 'd_2' : 20 mm

G. I pipe diameter, 'd_1' : 40 mm

Coefficient of discharge : 0.62

Length of the tube : 500 mm

OBSERVATION TABLE:

Sl. No	**Heater input Q (Watts)**			Diff. in Mano meter reading h_m mm	Air mass flow rate.	Tube surface Temperature °C					
	V volt	I amp	V X I			T_1	T_2	T_3	T_4	T_5	T_6
1.											
2.											
3.											

MODEL CALCULATIONS:

Method -I:

1. Velocity of the air in the tube $V_a = \dfrac{Q}{a_1}$

   Discharge of the air in the tube $Q = \dfrac{C_d a_1 a_2 \sqrt{2gh_m}}{\sqrt{a_1^2 - a_2^2}}$

   Where

   Coefficient of discharge C_d= 0.62

2. Properties of air are taken at temperature $T_f = \dfrac{T_h + T_s}{2}$

Average surface temperature of the tube $T_h = \frac{T_2 + T_3 + T_4 + T_5}{4}$

Mean temperature of air $T_s = \frac{T_1 + T_6}{2}$

3. Reynolds Number $R_e = \frac{V_a d_1}{\nu}$

   ($\nu = Kinematic Viscosity$ From data book at T_f)

4. Nusselt number Nu = 0.023 $R_e^{0.8}$ $P_r^{0.3}$

   (Pr= Prandtl number from data book at T_f)

5. Nusselt number $N_u = \frac{hd_1}{k}$

6. Forced convective heat transfer co-efficient $h = \frac{N_u k}{d_1}$ W/m² - K

   (k= thermal conductivity from data book at T_f)

Method -II:

From Newton's Law of Cooling:

1. Rate of heat transfer $Q = hA(T_h - T_s)$

   Where

   Amount of heat supplied Q = V X I Watts

   Surface area of the pipe $A = \prod d_1 L$

Forced convective heat transfer co-efficient $h = \frac{Q}{\prod d_1 L(T_h - T_s)}$ W/m² - K

PRECAUTIONS:

1. Never switch on main power supply before ensuring that all on/off switches given on the panel are at off position
2. Never run the apparatus if power supply is less than 180 or above 200 volts.

RESULT:

The convective heat transfer coefficient and the rate of heat transfer by forced convection for flow of air inside a horizontal pipe has been determined.

1. The convective heat transfer coefficient by forced convection h=………………

2. The rate of heat transfer by forced convection Q=………………………………..

Date:
Exp No:

HEAT TRANSFER BY NATURAL CONVECTION

AIM:

To find out heat transfer coefficient and heat transfer rate from vertical cylinder in natural convection.

THEORY:

Natural convection heat transfer takes place by movement of fluid particles on solid surface caused by density difference between the fluid particles on account of difference in temperature. Hence there is no external agency facing fluid over the surface. It has been observed that the fluid adjacent to the surface gets heated, resulting in thermal expansion of the fluid and reduction in its density. Subsequently a buoyancy force acts on the fluid causing it to flow up the surface. Here the flow velocity is developed due to difference in temperature between fluid particles.

The following empirical correlations may be used to find out the heat transfer coefficient for vertical cylinder in natural convection.

$$Nu = 0.53(Gr.\mathrm{Pr})^{\frac{1}{4}} \quad \textbf{for Gr.Pr<}10^5$$

$$Nu = 0.56(Gr.\mathrm{Pr})^{\frac{1}{4}} \quad \textbf{for } 10^5 < \textbf{Gr.Pr} < 10^8$$

$$Nu = 0.13(Gr.\mathrm{Pr})^{\frac{1}{3}} \quad \textbf{for } 10^8 < \textbf{Gr.Pr} < 10^{12}$$

Where,

Nu = Nusselt number = $\frac{hL}{k}$

Gr = Grashof number = $\frac{L^3 \beta g (T_S - T_a)}{\nu^2}$

Pr = Prandtl number = $\frac{\mu C_p}{k}$

β = Coefficient of Volumetric expansion (or) temperature co-efficient of thermal conductivity in $\frac{1}{K}$

For ideal gases $\beta = \frac{1}{T_f}$

Where 'T_f' is the absolute film temperature at which the properties are taken.

SPECIFICATIONS:

Specimen	: Stainless Steel tube,
Size of the Specimen	: Outer diameter 45mm, 500mm length
Heater	: Nichrome wire type heater along its length
Thermocouples used	: 6nos.
Ammeter	: Digital type, 0-2amps, AC
Voltmeter	: Digital type, 0-300volts, AC
Dimmer stat for heating coil	: 0-230 V, 2 amps, AC power
Enclosure with acrylic door	: For visual display of test section (fixed)

APPARATUS:

The apparatus consists of a stainless steel tube fitted in a rectangular duct in a vertical position. The duct is open at the top and bottom and forms an enclosure and serves the purpose of undisturbed surroundings. One side of the duct is made of acrylic sheet for visualization. A heating element is kept in the vertical tube, which heats the tube surface. The heat is lost from the tube to the surrounding air by natural convection. Digital temperature indicator measures the temperature at different points with the help of seven temperature sensors, including one for measuring surrounding temperature. The heat input to the heater is measured by Digital Ammeter and Digital Voltmeter and can be varied by a dimmer stat.

PROCEDURE:

1. Ensure that all ON/OFF switches given on the panel are at OFF position.
2. Ensure that variac knob is at zero position, provided on the panel.
3. Now switch on the main power supply (220 V AC, 50 Hz).

4. Switch on the panel with the help of mains ON/OFF switch given on the panel.
5. Fix the power input to the heater with the help of variac, voltmeter and ammeter provided.
6. Take thermocouple, voltmeter & ammeter readings when steady state is reached.
7. When experiment is over, switch off heater first.
8. Adjust variac to zero position.
9. Switch off the panel with the help of Mains On/Off switch given on the panel.
10. Switch off power supply to panel.

TABULAR COLUMN:

Sl. No.	V Volts	I Amps	Thermocouple readings °C					
			T_2	T_3	T_4	T_5	Chamber	
							Lower T_1	Upper T_6
1.								
2.								
3.								

CALCULATIONS:

1. Temperature of vertical cylinder wall $T_w = \frac{T_2+T_3+T_4+T_5}{4} + 273.15$ ^oK =………..

2. Surrounding ambient temperature $T_\infty = \frac{T_1+T_6}{2}$ =________+ 273.15 ^oK

3. Obtain the properties of air at a mean temperature of $T_f = \frac{T_w+T_\infty}{2}$ ^oK

4. Volumetric coefficient of thermal expansion $\beta = \frac{1}{T_f}$

5. Rayleigh Number Ra = Gr.Pr

6. Grashof Number, $Gr = \frac{L^3\beta g(T_w - T_\infty)}{\nu^2}$

Where,

Pr= Prandtl number (from Data book at T_f)………………

ν =kinematic viscosity……….. m^2/sec (from Data book at T_f)

7. Nusselt Number $Nu = \dfrac{hL}{k}$

The following correlations are used to find Nusselt Number

$$Nu = 0.53(Gr.Pr)^{\frac{1}{4}}$$ **for Gr.Pr<10^4**

$$Nu = 0.59(Gr.Pr)^{\frac{1}{4}}$$ **for 10^4<Gr.Pr<**10^9

$$Nu = 0.10(Gr.Pr)^{\frac{1}{3}}$$ **for 10^9<Gr.Pr**

8. Free convective heat transfer coefficient

$$h = \frac{Nu.k}{L} \quad W/m^2\text{–}K$$

9. Heat transfer rate by convection

$Q_c = h\ A\ (T_w - T_\infty)$

$Q_c = h\ \pi\ d\ L\ (T_w - T_\infty)$ watt

10. Heat Input to the coil

$Q_i = V \times I$ watts

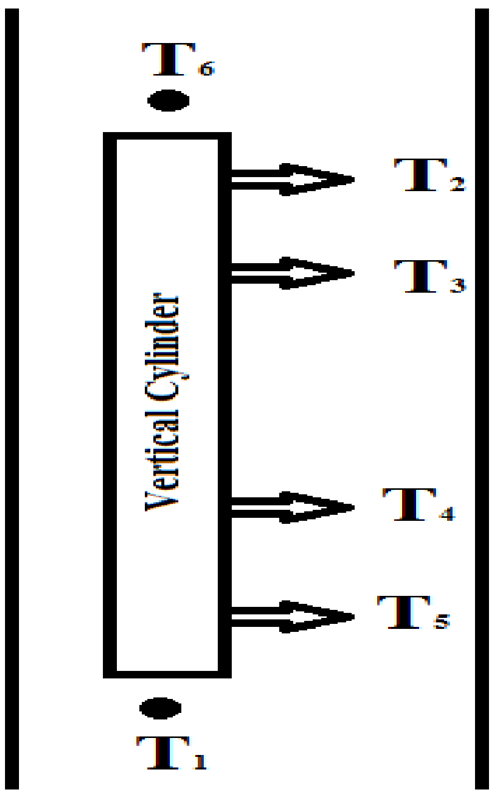


Fig: Natural Convection Apparatus

PRECAUTIONS:

1. Never switch on the main power supply before ensuring that all on / off switches give on the panel are at off position.
2. Never run the apparatus if power supply is less than 180 or above 200 Volts.
3. Make sure that convection should conduct in closed container.
4. Before switch on the main supply observer that the dimmer is in zero position.

RESULT:

The convective heat transfer coefficient and heat transfer rate from vertical cylinder in natural convection has been determined.

1. Convective heat transfer coefficient=…………………………..
2. Heat transfer rate=…………………………………

Date:
Exp No:

PARALLEL FLOW AND COUNTER FLOW HEAT EXCHANGER

AIM:

To determine LMTD, effectiveness and overall heat transfer coefficient for parallel and counter flow heat exchanger

SPECIFICATIONS:

Length of heat exchanger	L	=2440 mm
Inner copper tube	ID	=12 mm
	OD	=15 mm
Outer GI tube	ID	=40 mm
Geyser capacity		=1 Lt, 3 kW

THEORY:

Heat exchanger is a device in which heat is transferred from one fluid to another. Common examples of heat exchangers are:

i. Condensers and boilers in steam plant
ii. Inter coolers and pre-heaters
iii. Automobile radiators
iv. Regenerators

CLASSIFICATION OF HEAT EXCHANGERS:

1. **Based on the nature of heat exchange process:**
   i. Direct contact type – Here the heat transfer takes place by direct mixing of hot and cold fluids
   ii. Indirect contact heat exchangers – Here the two fluids are separated through a metallic wall. ex. Regenerators, Recuperators etc
2. **Based on the relative direction of fluid flow:**

i. Parallel flow heat exchanger – Here both hot and cold fluids flow in the same direction.

ii. Counter flow heat exchanger – Here hot and cold fluids flow in opposite direction.

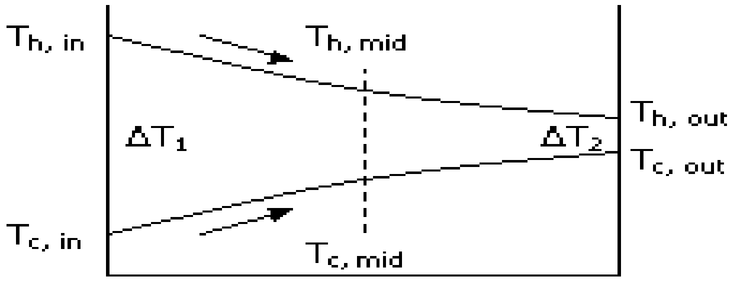
iii. Cross-flow heat exchangers – Here the two fluids cross one another.

LOGARITHMIC MEAN TEMPERATURE DIFFERENCE (LMTD):

This is defined as that temperature difference which, if constant, would give the same rate of heat transfer as usually occurs under variable conditions of temperature difference.

FOR PARALLEL FLOW:

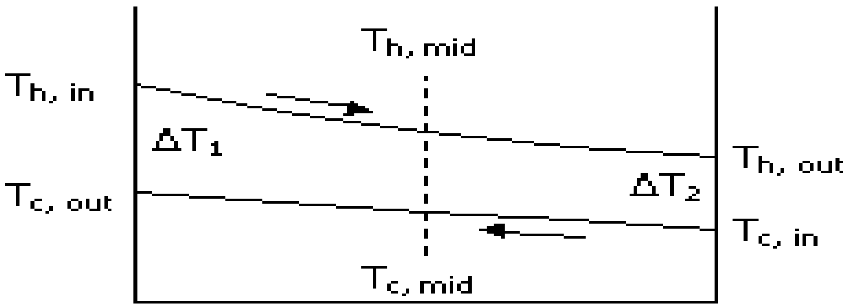
Where



Length of the TUBE

$$\textbf{LMTD} = \frac{(T_{ho} - T_{co}) - (T_{hi} - T_{ci})}{\ln\left(\frac{T_{ho} - T_{co}}{T_{hi} - T_{ci}}\right)} = \frac{\theta_2 - \theta_1}{\ln\left(\frac{\theta_2}{\theta_1}\right)}$$

For Counter flow:



Length of the TUBE

$$\text{LMTD} = \frac{(T_{hi} - T_{ci}) - (T_{ho} - T_{ci})}{\ln\left(\frac{T_{hi} - T_{co}}{T_{ho} - T_{ci}}\right)} = \frac{\theta_2 - \theta_1}{\ln\left(\frac{\theta_2}{\theta_1}\right)}$$

T_{ho} = Outlet temperature of hot fluid

T_{co} = Outlet temperature of cold fluid

T_{hi} = Inlet temperature of hot fluid

T_{ci} = Inlet temperature of cold fluid

OVERALL HEAT TRANSFER COEFFICINET:

The rate of heat transfer between hot and cold fluid is given by

$$Q = U_o A_o / LMTD$$

Where,

U_o is overall heat transfer coefficient based on outer surface area of tubes, W/m²-K

A_o is the total outer surface area of tubes, m²

EFFECTIVENESS:

Effectiveness of a heat exchanger is defined as the ratio of actual heat transfer rate to the theoretical maximum possible heat transfer rate.

Effectiveness: $\varepsilon = \frac{Q}{Q_{max}}$

It can be shown that

$$\varepsilon = \frac{T_{hi} - T_{ho}}{T_{hi} - T_{ci}} \quad \text{if } m_h c_h < m_c c_c$$

And

$$\varepsilon = \frac{T_{co} - T_{ci}}{T_{hi} - T_{ci}} \quad \text{if } m_c c_c < m_h c_h$$

Where,

m_h and m_c are the mass flow rate of hot and cold fluids respectively in kg/s;

c_h and c_c are the specific heat of hot and cold fluids respectively in J/kg–K.

DESCRIPTION OF THE APPRATUS:

The apparatus consists of a concentric tube heat exchanger. The hot fluid namely hot water is obtained from the Geyser (heater capacity 3 kW) & it flows through the inner tube. The cold fluid i.e. cold water can be admitted at any one of the ends enabling the heat exchanger to run as a parallel flow or as a counter flow exchanger. Measuring jar used for measure flow rate of cold and hot water. This can be adjusted by operating the different valves provided. Temperature of the fluid can be measured using thermocouples with digital display indicator. The outer tube is provided with insulation to minimize the heat loss to the surroundings.

PROCEDURE:

1. First switch ON the unit panel
2. Start the flow of cold water through the annulus and run the exchanger as counter flow or parallel flow.
3. Switch ON the geyser provided on the panel & allow to flow through the inner tube by regulating the valve.
4. Adjust the flow rate of hot water and cold water by using rotameters & valves.
5. Keep the flow rate same till steady state conditions are reached.
6. Note down the temperatures on hot and cold water sides. Also note the flow rate.
7. Repeat the experiment for different flow rates and for different temperatures. The same method is followed for parallel flow also.

OBSERVATION TABLE:

PARALLEL FLOW

Sl. No.	Hot water flow rate m_h, kg/s	Cold water flow rate m_c, kg/s	Temperature of cold water in °C		Temp. of hot water in °C	
			Inlet T_{ci}	Outlet T_{co}	Inlet T_{hi}	Outlet T_{ho}
1.						
2.						
3.						

COUNTER FLOW

Sl. No.	Hot water flow rate m_h, kg/s	Cold water flow rate m_c, kg/s	Temperature of cold water in °C		Temp. of hot water in °C	
			Inlet T_{ci}	Outlet T_{co}	Inlet T_{hi}	Outlet T_{ho}
1.						
2.						
3.						

EQUATIONS USED:

1. Heat transfer from hot water

$$Q_h = m_h C_{ph} (T_{hi} - T_{ho}) \text{ watts}$$

m_h = mass flow rate of hot water kg/sec
C_{ph} = Specific heat of hot water = 4186.8 J kg-K

2. Heat gain by the cold fluid

$$Q_c = m_c C_{pc} (T_{co} - T_{ci}) \text{ watts}$$

m_c = Mass flow of cold fluid, kg/s

C_{pc} = Specific heat of cold fluid = 4186.8 J/kg -K

3. $$Q = \frac{Q_h + Q_c}{2} \text{ watts}$$

$$LMTD = \frac{\theta_2 - \theta_1}{\ln\left(\frac{\theta_2}{\theta_1}\right)}$$

$\theta_1 = T_{hi} - T_{ci}$ and $\theta_2 = T_{ho} - T_{co}$ for parallel flow heat exchanger

$\theta_1 = T_{ho} - T_{ci}$ and $\theta_2 = T_{hi} - T_{co}$ for counter flow heat exchanger

5. Overall heat transfer coefficient based on outside surface area of inner tube

$$U_o = \frac{Q}{A_o . LMTD} \quad W/m^2\,{}^oK$$

Where,

A_o $= \pi d_o l$ m^2
d_o = Outer diameter of the tube = 0.0125 m
L = length of the tube = 1.5 m

6. Effectiveness:

Find $C_h = m_h c_{ph}$ and $C_c = m_c c_{pc}$

Effectiveness = $\dfrac{T_{hi} - T_{ho}}{T_{hi} - T_{ci}}$ if $C_h < C_c$

And Effectiveness = $\dfrac{T_{co} - T_{ci}}{T_{hi} - T_{ci}}$ if $C_c < C_h$

This is applicable both for Parallel and counter flow heat exchanger

7. Effectiveness using NUMBER OF TRANSFER UNIT (NTU) method

i) NTU = $\dfrac{U_o A_o}{C_{min}}$

Note: if $C_h < C_c$ then $C_h = C_{min}$, $C_c = C_{max}$

And if $C_c < C_h$ then $C_c = C_{min}$, $C_h = C_{max}$

ii) Effectiveness of parallel flow heat exchanger

$$\varepsilon = \frac{1 - e^{-NTU\left[1 + \frac{C_{min}}{C_{max}}\right]}}{1 + \frac{C_{min}}{C_{max}}}$$

iii) Effectiveness of counter flow heat exchanger

$$\varepsilon = \frac{1 - e^{-NTU\left[1 - \frac{C_{min}}{C_{max}}\right]}}{1 - \frac{C_{min}}{C_{max}} e^{-NTU\left[1 - \frac{C_{min}}{C_{max}}\right]}}$$

RESULT:

The overall heat transfer coefficient of parallel flow and counter flow heat exchangers has been determined.

Date:
Exp No:

HEAT TRANSFER FROM PIN-FIN APPARATUS

AIM:

To determine the temperature of a pin-fin for forced convection and to find fin efficiency and effectiveness.

SPECIFICATIONS:

Length of the fin, ‘L’	= 145mm
Diameter of the fin, ‘d_f’	= 12mm
Diameter of the orifice, ‘d_o’	= 20 mm
Width of the duct, ‘W’	= 150 mm
Breadth of the duct, ‘B’	= 100 mm
Coefficient of discharge of the orifice, ‘C_d’	= 0.62
Density of manometric fluid (water)	=1000 kg/m^3

THEORY:

The heat transfer from a heated surface to the ambient surrounding is given by the relation, $q = h\ A\ \Delta T$. In this relation h_c is the convective heat transfer coefficient, ΔT is the temperature difference & A is the area of heat transfer. To increase q, h may be increased or surface area may by increased. In some cases it is not possible to increase the value of heat transfer coefficient & the temperature difference ΔT & thus the only alternative is to increase the surface area of heat transfer. The surface area is increased by attaching extra material in the form of rod (circular or rectangular) on the surface where we have to increase the heat transfer rate. "This extra material attached is called the extended surface or fin."

The fins may be attached on a plane surface, and then they are called plane surface fins. If the fins are attached on the cylindrical surface, they are called circumferential fins. The cross section of the fin may be circular, rectangular, triangular or parabolic.

Temperature distribution along the length of the fin:

$$\frac{\theta}{\theta_0} = \frac{T - T_\infty}{T_0 - T_\infty} = \frac{\cosh[m(L-x)]}{\cosh(mL)}$$

Where

T = Temperature at any distance x on the fin

T_0 = Temperature at x = 0

T_∞ = Ambient temperature

L = Length of the fin

$$m = \sqrt{\frac{h_c P}{kA}}$$

Where

h = convective heat transfer coefficient

P = Perimeter of the fin

A = area of the fin

K = Thermal conductivity of the fin

Rate of heat flow for end insulated condition:

$$Q = \theta_0 \sqrt{h_c PkA} \tanh(mL)$$

Effectiveness of a fin is defined as the ratio of the heat transfer with fin to the heat transfer from the surface without fins.

$$\varepsilon = \frac{\theta_0\left(\sqrt{hPkA}\right)\tanh(mL)}{hA\theta_0}$$

$$\varepsilon = \left(\sqrt{\frac{Pk}{hA}}\right)\tanh(mL)$$

The efficiency of a fin is defined as the ratio of the actual heat transferred by the fin to the maximum heat transferred by the fin if the entire fin area were at base temperature.

$$\eta_f = \frac{\theta_0\left(\sqrt{hPkA}\right)\tanh(mL)}{hPL\theta_0}$$

$$\eta_f = \frac{\tanh(mL)}{mL}$$

PROCEDURE:

1. Connect the equipment to electric power supply.
2. Keep the thermocouple selector switch to zero position.

3. Turn the dimmer stat clockwise and adjust the power input to the heater to the desired value and switch on the blower.
4. Set the air–flow rate to any desired value by adjusting the difference in water levels in the manometer and allow the unit to stabilize.
5. Note down the temperatures, T_1 to T_6 from the thermocouple selector switch.

Note down the difference in level of the manometer and repeat the experiment for different power inputs to the heater.

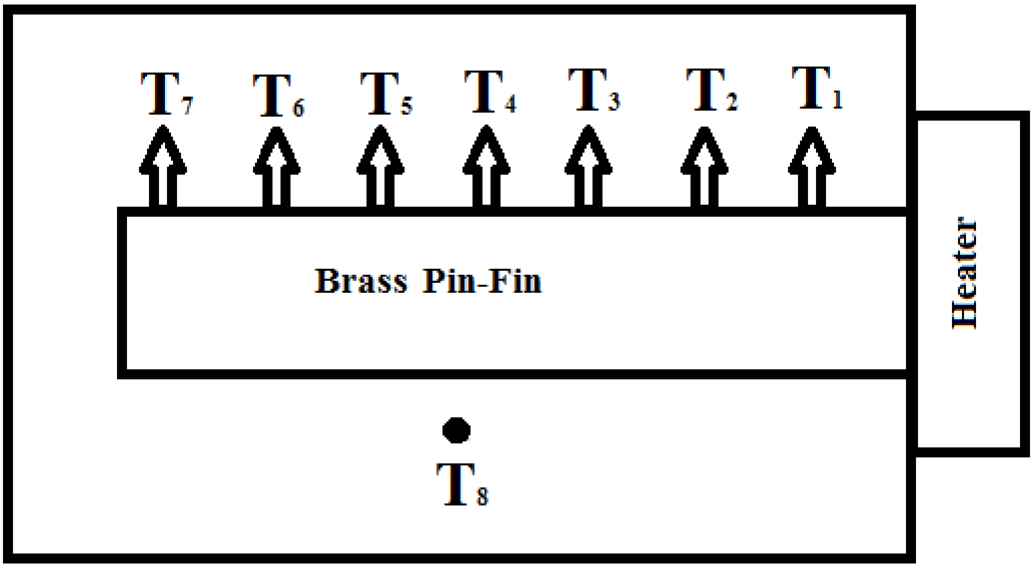


Fig: Pin-Fin apparatus

CALCULATIONS:

7. Velocity of the air in the tube $V_a = \dfrac{Q}{a_1}$

Discharge of the air in the tube $Q = \dfrac{C_d a_1 a_2 \sqrt{2gh_m}}{\sqrt{a_1^2 - a_2^2}}$

Where

Coefficient of discharge C_d= 0.62

Area of Pipe $a_1 = \dfrac{\Pi}{4} d_1^2$ →d_1 is diameter of the pipe = 40mm.

Area of Orifice $a_2 = \dfrac{\Pi}{4} d_2^2$ →d_2 is diameter of the Orifice = 20mm.

h_m Differential manometer reading .

8. Properties of air are taken at temperature $T_f = \dfrac{T_w + T_\infty}{2}$

Where

Average surface temperature of the Pin-fin

$$T_{avg} = T_w = \frac{T_1 + T_2 + T_3 + T_4 + T_5 + T_6 + T_7}{7}$$

Ambient temperature of air in Duct $T_\infty = T_8$

9. Reynolds Number $$Re_D = \frac{V_a . d_f}{\nu}$$

($\nu = Kinematic Viscosity$ From data book at T_f)

(Pr= Prandtl number from data book at T_f)

10. Nusselt number **Nu =** $C \, Re_D^{\,m} \, Pr^{\,0.333}$

For

Re_D = 0.4	to 4.0	C = 0.989	m = 0.33
Re_D = 4	to 40	C = 0.911	m = 0.385
Re_D = 40	to 4000	C = 0.683	m = 0.466
Re_D = 4000	to 40,000	C = 0.293	m = 0.618
Re_D = 40,000	to 400,000	C = 0.27	m = 0.805

11. Nusselt number $$Nu = \frac{h d_f}{k}$$

12. Forced convective heat transfer co-efficient $$h = \frac{N_u k}{d_f}$$ W/m² - K

(k= thermal conductivity from data book at T_f)

13. Rate of heat transfer $Q_c = h\,A\,(T_w - T_\infty)$

$Q_c = h\,\pi\,d\,L\,(T_w - T_\infty)$ watt

14. Temperature distribution is given by

$$\frac{T - T_\infty}{T_0 - T_\infty} = \frac{\cosh(m(L - X))}{\cosh(mL)}$$

15. Therefore $$T = T_8 + [T_1 - T_8] \times \left[\frac{\cosh(m(L - X))}{\cosh(mL)}\right]$$

Distance x, m	Temperature from Experiment °C	Temperature °C from calculation
x_1 = 0.02	$T_{0.02}$=	$T_{0.02}$=
x_2 =0.04	$T_{0.04}$=	$T_{0.04}$=
x_3 =0.06	$T_{0.06}$=	$T_{0.06}$=
x_4 = 0.08	$T_{0.08}$=	$T_{0.08}$=
x_5 =0.10	$T_{0.1}$=	$T_{0.1}$=

$x_6 = 0.12$	$T_{0.12}=$	$T_{0.12}=$
$x_7 = 0.14$	$T_{0.14}=$	$T_{0.14}=$

16. Efficiency of fin $\eta_f = \dfrac{\tanh(mL)}{mL}$

Where L= Length of the Fin= 145mm

$$m = \sqrt{\frac{hP}{k_{brass}A}}$$

h= Convective heat transfer coefficient w/m^2-K

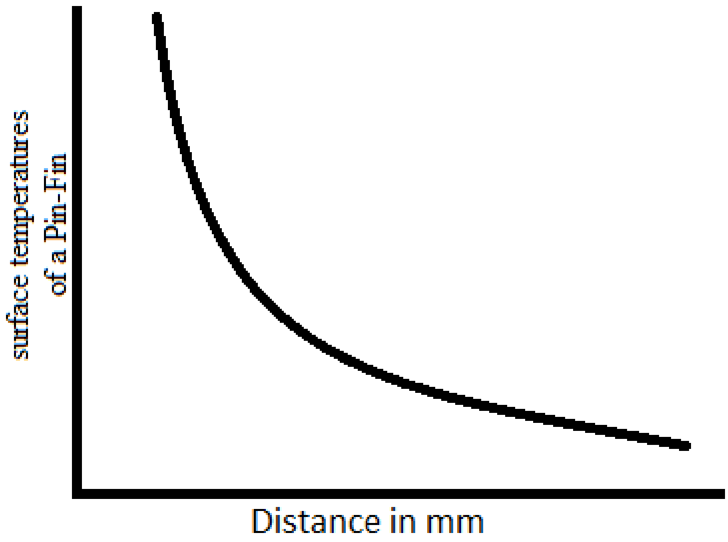
P= Perimeter of the Fin (πd_f)

A= Cross-sectional area of the Fin $A = \dfrac{\Pi}{4} d_f^2$

k_{brass}= Thermal conductivity of brass =110.7 W/m-K

17. Effectiveness of fin $\varepsilon = \left(\sqrt{\dfrac{Pk}{hA}}\right) \tanh(mL)$

<u>GRAFF:</u> surface temperature of Pin-Fin Vs Distance (location of thermocouples on Pin-Fin)



<u>PRECAUTIONS</u>:

3. Never switch on main power supply before ensuring that all on/off switches given on the panel are at off position
4. Never run the apparatus if power supply is less than 180 or above 200 volts.

<u>RESULT</u>:

The temperature distribution of a pin – fin for forced convection efficiency and effectiveness has been determined.

1. Temperature distribution of a pin fin is given by

Distance x, m	Temperature from Experiment °C	Temperature °C from calculation
$x_1 = 0.02$	$T_{0.02}$=	$T_{0.02}$=
$x_2 = 0.04$	$T_{0.04}$=	$T_{0.04}$=
$x_3 = 0.06$	$T_{0.06}$=	$T_{0.06}$=
$x_4 = 0.08$	$T_{0.08}$=	$T_{0.08}$=
$x_5 = 0.10$	$T_{0.1}$=	$T_{0.1}$=
$x_6 = 0.12$	$T_{0.12}$=	$T_{0.12}$=
$x_7 = 0.14$	$T_{0.14}$=	$T_{0.14}$=

2. Efficiency of Pin-Fin=……………………………

3. Effectiveness of Pin-Fin=…………………………

Date:
Exp No:

STEFAN BOLTZMANN APPARATUS

AIM:

To determine the value of Stefan Boltzmann constant for radiation heat transfer.

APPARATUS:

Hemisphere, Heater, Temperature indicator, Stopwatch.

THEORY:

Stefan Boltzmann law states that the total emissive power of a perfect black body is proportional to fourth power of the absolute temperature of black body surface.

$$E_b = \sigma T^4$$

Where

σ = Stefan Boltzmann constant = 5.6697×10^{-8} W/(m^2 K^4)

DESCRIPTION:

The apparatus consists of a flanged copper hemisphere fixed on a flat non-conducting plate. A test disc made of copper is fixed to the plate. Thus the test disc is completely enclosed by the hemisphere. The outer surface of the hemisphere is enclosed in a vertical water jacket used to heat the hemisphere to a suitable constant temperature. Three Cr-Al thermocouples are attached at three strategic places on the surface of the hemisphere to obtain the temperatures. The disc is mounted on an ebonite rod which is fitted in a hole drilled at the center of the base plate. Another Cr-Al thermocouple is fixed to the disc to record its temperature. Fill the water in the SS water container with immersion heater kept on top of the panel.

SPECIFICATIONS:

Specimen material	:	Copper
Size of the disc	:	ϕ 20mm x 0.5mm thickness
Base Plate	:	ϕ 250mm x 12mm thickness (hylam)

Heater	:	1.5 kW capacity, immersion type
Copper Bowl	:	ϕ 200mm
Digital temperature indicator	:	0 -199.9° C
Thermocouples used	:	3 nos. on hemisphere
Stop Watch	:	Digital type
Overhead Tank	:	SS, approx. 12 liter capacity
Water Jacket	:	ϕ 230 mm, SS
Mass of specimen, 'm'	:	5 gm
Specific heat of the disc C_p	:	0.38 kJ/kg K

PROCEDURE:

1. Remove the test disc before starting the experiment.
2. Allow water to flow through the hemisphere, Switch on the heater and allow the hemisphere to reach a steady state temperature.
3. Note down the temperatures T_1,T_2 & T_3. The average of these temperatures is the hemisphere temperature T_h .
4. Insert the test disc at the bottom of the hemisphere and lock it. Start the stop clock simultaneously.
5. Note down the temperature of the test disc at an interval of about 15 sec for about 15 to 20 minutes.

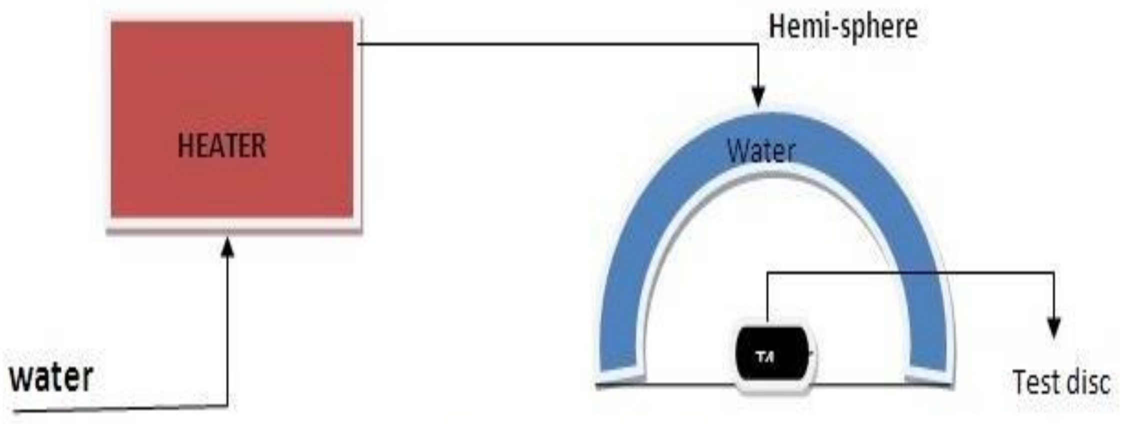


FIG: STEFAN BOLTZMANN APPARATUS

OBSERVATION TABLE:

Let T_d = Temperature of the disc before inserting into the plate in K

Thermocouple	Temperature of the copper hemisphere ° C
T_1	
T_2	
T_3	
T_h Average of T_1 , T_2 and T_3 =	

Temperature – time response of test disc:

Time 't' sec	Temperature T_d ° C	Time 't' sec	Temperature T_d ° C

CALCULATIONS:

1. Plot the graph of temperature of the disc v/s time to obtain the slope (dT/dt) of the line, which passes through/nearer to all points.
2. Average temperature of the hemisphere

$$T_h = \frac{T_1 + T_2 + T_3}{3} + 273.15$$

3. T_d = Temperature of the disc before inserting to Test chamber ^{o} K (ambient)

4. Rate of change of heat capacity of the disc = $mC_p \frac{dT}{dt}$

Net energy radiated on the disc = $\sigma A_d (T^4_h - T^4_d)$

Where

A_d = area of the disc = $\frac{\pi}{4} d^2$ in m^2

d = 20 mm

C_p = specific heat of copper = 0.38 kJ/kg–K

Rate of change of heat capacity of the disc = Net energy radiated on the disc

$$mC_p \frac{dT}{dt} = \sigma A_d (T^4_{avg} - T^4_d)$$

Thus 'σ' can be evaluated as shown

$$o = \frac{mC_p \frac{dT}{dt}}{A_d (T^4_{avg} - T_d^4)}$$

Result: The experiment on Stefan Boltzmann apparatus has been conducted and the value of Stefan Boltzmann constant is determined.

Date:
Exp No:

THERMAL CONDUCTIVITY OF METAL ROD

AIM:

To determine the thermal conductivity of given metal rod.

THEORY:

From Fourier's law of heat conduction

$$Q = -kA\frac{dT}{dx}$$

where

Q = Rate of heat conducted, W

A = Area of heat transfer, m^2

k = Thermal conductivity of the material, W/m-K

$\frac{dT}{dx}$ = Temperature gradient

Thermal conductivity is a property of the material and may be defined as the amount of heat conducted per unit time through unit area, when a temperature difference of unit degree is maintained across unit thickness.

DESCRIPTION OF THE APPARATUS:

The apparatus consists of a brass rod, one end of which is heated by an electric heating coil while the other end projects into the cooling water jacket. The rod is insulated with glass wool to minimize the radiation and convection loss from the surface of the rod and thus ensure nearly constant temperature gradient throughout the length of the rod. The temperature of the rod is measured at five different locations. The heater is provided with a dimmerstat for controlling the heat input. Water is circulated through the jacket and its flow rate and temperature rise can be measured.

SPECIFICATIONS :

Specimen material	:	Brass rod
Size of the Specimen	:	ϕ20 mm, 450mm long
Cylindrical shell	:	300mm long

Voltmeter	:	Digital type, 0-300volt, AC
Ammeter	:	Digital type, 0-20amp, AC
Dimmer for heating Coil	:	0-230v, 12amps
Heater	:	Band type Nichrome heater, 250 W
Thermocouple used	:	11 nos.
Temperature indicator	:	Digital type, 0-200^{0}c, Cr-Al

PRODEDURE:

1. Power supply is given to the apparatus.
2. Give heat input to the heater by slowly rotating the dimmer and adjust the voltage to say 60 V, 80 V, etc
3. Start the cooling water supply through the jacket and adjust its flow rate so that the heat is taken away from the specimen constantly.
4. Allow sufficient time for the apparatus to reach steady state.
5. Take readings of voltmeter and ammeter.
6. Note the temperatures along the length of the specimen rod at 5 different locations.
7. Note down the inlet & outlet temperatures of cooling water and measure the flow rate of water.
8. Repeat the experiment for different heat inputs.

OBSERVATION TABLE:

'V' Volt	'I' Amp	Metal rod thermocouple reading (0C)									Water temp (0C)		Volume flow rate of water, V cc/min
											In let	Ou tlet	
		T_1	T_2	T_3	T_4	T_5	T_6	T_7	T_8	T_9	T_{10}	T_{11}	
1.													
2.													
3.													

CALCULATION:

Plot the variation of temperature along the length of the rod. From the graph, obtain dT/dx, which is the slope of the straight line passing through/near to the points in the graph. Assuming no heat loss, heat conducted through the rod = heat carried away by the cooling water

$$kA\frac{dT}{dx} = m_f C_p (T_{11} - T_{10})$$

Where, 'k' = thermal conductivity of metal rod, (W/m-K)

'A' = Cross sectional area of metal rod = $\pi d^2/4$ (m^2)

'd' = diameter of the specimen = 20 mm

'C_p' = Specific heat of water = 4.187 kJ/kg-K

Thus, the thermal conductivity 'k' of metal rod can be evaluated.

$$k = \frac{m_f C_p (T_{11} - T_{10})}{A\frac{dT}{dx}}$$

GRAPH:

Plot the graph Distance vs Temperature.

PRECAUTIONS:

7. Keep the dimmer stat to zero before starting the experiment.
8. Take readings at study state condition only.
9. Use the selector switch knob and dimmer knob gently.

RESULT:

The thermal conductivity of given metal rod has been determined.
flux and temperature.

Date:

Exp No:

UNSTEADY STATE HEAT TRANSFER

AIM:

To obtain the specimen temperature at any interval of time by theoretical methods and observe the heating and cooling curves of unsteady state.

INTRODUCTION:

Unsteady state designates a phenomenon which is time dependent. Conduction of heat in unsteady state refers to transient conditions where in, heat flow and temperature distribution at any point of system varies with time. Transient conditions occur in heating or cooling of metal billets, cooling of IC engine cylinder, brick and vulcanization of rubber.

DESCRIPTION:

Unsteady state heat transfer equipment has oil check which is at top of oil heater. Thermocouple No.1is located inside the specimen No.2 thermocouple measures the atmospheric temperature. No.3 thermocouple measures the oil temperature.

Digital temperature indicator indicates respective temperatures of thermocouples as we select it by selector switch. Heater ON/OFF toggle switch and buzzer ON/OFF toggle switch is provided on the control panel.

SPECIFICATIONS:

1. D.C Buzzer : 10-30 volt
2. Oil Heater : 1 kW
3. Digital temperature indicator : $1200C^0$
4. Thermocouple : Al-Cr type
5. Specimens material : Copper
6. Fuse : 4 Amps.

EXPERIMENTATION:

Obtain the specimen temperature at any interval of time by practical and by theoretical methods and observe the heating and cooling curves of unsteady state.

PROCEDURE:

1. Put ON the mains switch.
2. Fill the oil jar up to $\frac{3}{4}^{th}$ of its height.
3. Insert the thermocouple in jar having tag No.3.
4. Keep thermocouple No.2 near to the specimen inside the transparent chamber.
5. Start the oil heater by putting heater's toggle switch in downward direction.
6. Keep selector switch No.3 and observe oil temperature.
7. When the oil temperature reaches up to 95^0C insert specimen in oil jar. At the same time note down the specimen temperature and start the stop watch.
8. Note down the specimen reading for every 30 sec. Check the oil temperature by selecting No.3 on selector switch.
9. Take the readings of specimen temperature till it comes nearly too hot oil temperature.
10. Now put the specimen inside the rectangular chamber. At the same timed put OFF the heater.
11. Take the atmospheric temperature by selecting No.2 and specimen temperature. Note the specimen temperature reading till it comes closer to atmospheric temperature.
12. Put OFF the main switch.

OBSERVATIONS:

1. Specimen material : Copper
2. Thermal conductivity of copper, $k=386\ W/m^0k$.
3. Coefficient of thermal expansion $a=17.7x10^{-6}/^0C$
4. Specimen diameter, d=30mm
5. Specimen lengh, l=30mm

TABULATION:

In case of Heating:

Sl. No	Oil temperature T_1 in ^0C	Specimen Temperature T_3 in ^0C at interval of 30 sec.	Time in second t
1.	70		0
2.			30
3.			60
4.			90
5.			120
6.			150
7.			180
8.			240
9.			270
10.			300
11			330

In case of Cooling:

Sl. No	Atmospheric temperature T_2 in ^0C	Specimen Temperature T_3 in ^0C at interval of 30 sec	Time in second t
1.			0
2.			30
3.			60
4.			90
5.			120
6.			150
7.			180
8.			240
9.			270
10.			300
11			330

CALCULATION:

Specimen material : Copper

Thermal conductivity of copper, $k=386\ W/m^0k$.

Coefficient of thermal expansion $a=17.7x10^{-6}/^0C$

Specimen diameter, d=30mm

Specimen length, l=30mm

Characteristic length for cylinder L= d/2

Biot number $Bi=\frac{hL}{k}$

Fourier number $Fo=\frac{\alpha t}{L^2}$

Mean temperature = $T = \frac{T_{max} + T_{min}}{2}$

In case of cooling

T_{max}=specimen temperature just after the hot oil both

Tmin= atmosperic temperature

In case of heating

T_{max}=hot oil temperature

T_{min}= specimen temperature before inserting into oil both

$$\frac{T - T_{\infty}}{T_0 - T_{\infty}} = e^{-(Bi...X..Fo)}$$

Where

T= temperature of the specimen at time interval of ‘t’ sec

T_a= atmospheric temperature in 0C

T_s=specimen temperature

In case of cooling

Ta= atmospheric temperature

T_s= specimen temperature

In case of heating

T_a= Specimen temperature

T_s= hot oil temperature

Obtain the temperature at any desired interval of the time

Plot the graph of temperature difference V/S time for heating and cooling

PRECAUTIONS:

1. Keep the dimmer stat to zero before starting the experiment.
2. Operate the stop watch carefully.
3. Use the selector switch knob and dimmer knob gently.

RESULT:

The specimen temperature at an interval of time by practical and by theoretical methods and observe the heating and cooling curves of unsteady state is observed.